FCCU Process Description

The Fluidized Catalytic Cracking Unit (FCCU) is a refinery process unit used for the production of gasoline. Heavy oil, which is used as the feedstock, is catalytically cracked in a fluidized catalyst bed to produce C3 olefins, C4 olefins, and isobutanes. In the cracking reactor, heavy carbonaceous materials (coke) become deposited on the catalyst, requiring continuous regeneration. The catalyst is circulated to a fluidized bed regenerator where these deposits are combusted. Most of the catalyst particles entrained in the regenerator flue gas are then removed in two stages of cyclones within the regenerator vessel and then are returned to the fluidized bed reactor.

At the Trainer Refinery, the FCCU control devices include a CO Boiler for CO reduction, an Enhanced Selective Non-Catalytic Reduction (eSNCR) unit for NO_x reduction, an electrostatic precipitator for PM reduction and a wet gas scrubber for PM and SO_2

Catalytic Reforming Unit (Platformer Unit)

The refinery operates one Catalytic Reforming Unit. The purpose of the Platformer is to upgrade low octane feed sources, Heavy Naphtha and Heavy Isocrackate, into a high-octane gasoline component and hydrogen gas. The feed combined with hydrogen recycle gas is heated and passed over a platinum catalyst, where it is converted from low octane naphtha to a gasoline-blending component with a design research octane number in the range of 97 - 101.

SRU

The Claus Sulfur Recovery Unit is designed to react feed H_2S and SO_2 into recoverable sulfur using two trains in parallel. Normally only one train is required to be on-line. The feeds to the unit are sour water gases and acid gases from the Sour Water Stripper and the Amine Unit. Each train consists of a thermal reactor, three catalytic reactors, a steam generator and a 4 pass sulfur condenser. Medium and low-pressure steam is generated in the condensers. The sulfur product is stored in a common heated pit until shipped out by railcar.

The Scot unit is designed to treat the tail gas from both trains of the Sulfur Recovery Unit. The Scot Unit reduces the H_2S content in the tail gas before it is sent to the incinerator stack. The combination of the Sulfur and Scot Units recovers about 99.8% of the sulfur in the feed streams. The Scot Unit consists of an in-line burners, catalytic reactor, quench tower, amine absorber, stripper, and incinerator.

Bypass Lines

The FCCU does not have any bypass lines. The Platformer Chlorsorb Unit line was not bypassed during this reporting period. The Sulfur Recovery Unit line was not bypassed during this reporting period.

Attachment 4 – Excess Emissions and Monitoring Systems Performance Report (40 CFR 60.7 (c))

Main Flare Excess Emissions Report

Start Date/Time	End Date/Time	Magnitude of Emissions (ppm H ₂ S)	SSM Related?	Nature and Cause of Malfunction	Corrective Action Taken/Preventative Measures
01/01/15 00:00	01/07/15 23:00	170.4-603.9			
01/08/15 09:00	01/08/15 10:00	167.0			
01/08/15 13:00	01/10/15 08:00	165.1-669.5			
01/10/15 14:00	01/13/15 00:00	168.0-553.4			
01/13/15 01:00	01/20/15 00:00	164.5-1336.6			
01/20/15 10:00	01/20/15 13:00	163.5-175.8			
01/20/15 10:00	01/21/15 17:00	166.7-181.7			
01/21/15 17:00	01/28/15 07:00	166.8-472.6			
01/28/15 11:00	01/28/15 20:00	172.9-228.6			
01/30/15 05:00	01/30/15 07:00	179.0-255.5			
01/30/15 14:00	02/07/15 10:00	190.9-801.9			
02/07/15 22:00	02/16/15 17:00	162.4-819.2			
02/17/15 13:00	02/18/15 06:00	166.0-750.4			
02/18/15 08:00	02/21/15 06:00	172.6-1847.3			
02/21/15 12:00	02/22/15 06:00	168.4-1906.7			
02/22/15 08:00	02/22/15 11:00	172.5-189.1			
02/23/15 00:00	02/23/15 08:00	178.7-381.3	4		
02/23/15 16:00	02/24/15 15:00	217.0-798.4			
02/24/15 21:00	02/25/15 12:00	177.7-221.1	1	1	
02/25/15 14:00	02/25/15 19:00	164.5-176.7			
02/26/15 03:00	02/26/15 12:00	172.8-212.1			
02/26/15 19:00	02/27/15 00:00	164.8-191.9	4		
02/27/15 07:00	02/28/15 14:00	225.6-893.8	1		Flare Gas Recover
02/28/15 15:00	02/28/15 17:00	165.6-171.5	No	N/A	Unit Was installed
02/28/15 21:00	03/01/15 07:00	191.7-407.9	_		Offic was mistanes
03/01/15 11:00	03/03/15 07:00	332.7-1561.0			
03/03/15 11:00	03/09/15 09:00	194.7-2007.1	-		
03/09/15 13:00	03/10/15 03:00	171.5-322.7			
03/10/15 07:00	03/13/15 05:00	175.4-1173.1			
03/13/15 11:00	03/13/15 12:00	162.3			
03/13/15 17:00	03/13/15 21:00	172.1-207.2	_		
03/16/15 09:00	03/16/15 12:00	207.0-270.8	4		
03/16/15 18:00	03/17/15 00:00	168.8-247.8	4		
03/17/15 04:00	03/17/15 06:00	176.8-181.2	-		
03/18/15 08:00	03/18/15 13:00	164.7-210.5	-		4
03/20/15 15:00	03/23/15 19:00	165.2-765.3			
03/23/15 20:00	03/23/15 21:00	163.7	-		
03/23/15 22:00	03/23/15 23:00	166.4	_		
03/24/15 00:00	03/24/15 03:00	167.1-173.3		1	
03/24/15 13:00	03/24/15 15:00	163.8-165.9			
03/24/15 20:00	03/24/15 22:00	162.4	-		
03/25/15 05:00	03/25/15 06:00	163.3			
03/25/15 14:00	03/25/15 21:00	165.4-234.1			
03/26/15 09:00	03/26/15 16:00	166.3-171.6	Special Control of the Control of th		
03/26/15 22:00	03/27/15 04:00	164.8-169.8	•		
03/27/15 10:00	03/27/15 11:00				
03/29/15 09:00	04/02/15 09:00		50,000,000		
04/02/15 22:00	04/04/15 09:00	171.9-296.0			

Start Date/Time	End Date/Time	Magnitude of Emissions (ppm H ₂ S)	SSM Related?	Nature and Cause of Malfunction	Corrective Action Taken/Preventative
04/06/15 10:00	04/06/15 23:00	166.7-388.7		ivialiunction	Measures
04/09/15 00:00	04/09/15 04:00	206.2-484.4			
04/09/15 14:00	04/09/15 17:00	164.2-202.4			
04/09/15 21:00	04/10/15 03:00	183.1-234.4			
04/10/15 08:00	04/10/15 16:00	172.6-372.6			
04/10/15 19:00	04/11/15 06:00	167.1-272.1			
04/12/15 08:00	04/12/15 14:00	186.0-272.1			
04/12/15 15:00	04/12/15 23:00	164.0-189.4			
04/13/15 11:00	04/17/15 07:00	165.8-620.6			
04/17/15 10:00	04/21/15 07:00	163.6-657.0			
04/21/15 17:00	04/22/15 01:00	164.9-400.3			
04/22/15 13:00	04/22/15 17:00	192.7-282.5			
04/23/15 06:00	04/23/15 08:00	178.8			
04/23/15 14:00	04/23/15 21:00	168.3-204.9			
04/24/15 02:00	04/24/15 09:00	168.7-203.3			
04/24/15 15:00	04/25/15 10:00	165.3-391.8			
04/25/15 13:00	04/27/15 21:00	172.5-560.5	1		
04/28/15 01:00	04/29/15 20:00	170.1-279.8	1	-	
04/29/15 21:00	04/30/15 09:00			1	
04/30/15 20:00	04/30/15 21:00	166.2-216.1			
04/30/15 01:00	05/07/15 11:00	170.3			
05/07/15 12:00	05/13/15 11:00	163.9-572.6			
05/13/15 16:00	05/13/15 17:00	162.3-1153.4			
05/13/15 20:00	05/14/15 10:00	163.0			Flare C. D
05/15/15 18:00	05/15/15 20:00	164.1-233.6	No	N/A	Flare Gas Recovery
05/16/15 18:00	05/18/15 20:00	178.6-179.1	1		Unit Was installed.
05/20/15 16:00	05/21/15 09:00	173.8-1346.5			
05/22/15 18:00	05/23/15 18:00	172.5-239.6	1		
05/24/15 14:00	05/24/15 16:00	167.0-416.1			
5/24/15 18:00	05/25/15 21:00	171.4-175.2			
5/26/15 00:00	05/29/15 21:00	168.0-237.0			
5/29/15 23:00	05/30/15 19:00	166.0-536.7			
5/30/15 21:00	06/01/15 20:00	168.1-268.2			
6/02/15 04:00	06/02/15 15:00	166.8-1100.2			
6/03/15 06:00	06/02/15 15:00	163.5-200.3			
6/03/15 11:00	06/06/15 10:00	167.7			
6/06/15 14:00	06/15/15 04:00	171.6-857.1			
5/15/15 15:00		165.2-1160.4			
5/17/15 17:00	06/17/15 11:00	166.4-798.9			
5/18/15 09:00	06/18/15 04:00	166.7-224.2			
5/20/15 16:00	06/20/15 12:00	166.5-647.5			
5/21/15 14:00	06/21/15 10:00	183.8-407.3	-		
6/24/15 03:00	06/24/15 01:00	171.5-559.7			
1	06/26/15 00:00	162.1-716.8			
	06/26/15 21:00	167.1-367.6	1		
10=1	06/27/15 10:00	165.6-173.5			
107145	06/27/15 13:00	218.4-424.1			
/27/15 16:00	07/01/15 00:00	244.9-823.0			

42-045-00070



Monroe Energy, LLC 4101 Post Road Trainer, PA 19061 (610) 364-8000

November 9, 2016

FedEx 7774 1757 8567

Mr. James Rebarchak Commonwealth of Pennsylvania Department of Environmental Protection Southeast Regional Office 2 East Main Street Norristown, PA 19401

Re:

Monroe Energy, LLC - Trainer Refinery

40 CFR 63, Subpart UUU: Revised Semi-Annual Periodic Report

40 CFR 60, NSPS J: Revised Semi-Annual Report Reporting Period: July 1, 2014– December 31, 2014

Dear Mr. Rebarchak:

In accordance with 40 CFR Part 60 Subpart J and 40 CFR 63 Subpart UUU, Monroe Energy, LLC's Trainer Refinery hereby submits this revised semi-annual compliance report (per §63.1575(b)(2)) for the period beginning July 1, 2014– December 31, 2014.

Should you have any questions or comments regarding this revised report, please contact Mr. Matthew Torell, P.E. Environmental Leader, at (610) 364-8399.

Sincerely,

Haley Ilg

Air Permit Compliance Lead

Enclosure

FedEx 7774 1780 2870

U.S. EPA, Region III Director, Air Protection Division Mail Code 3AP20 1650 Arch Street Philadelphia, Pa 19103-2029

Responsible Official Certification

Based upon information and belief formed after a reasonable inquiry, I, as a responsible official of the above-mentioned facility, certify the information contained in this report is accurate and true to the best of my knowledge.

Jeffrey K. Warmann, CEO & President

REVISED SEMIANNUAL PERIODIC REPORT Reporting Period: July 1, 2014 – December 31, 2014

40 CFR Part 63 Subpart UUU

The Refinery MACT 2 emission standards regulate the following refinery affected sources and parameters:

- 1) Fluidized Catalytic Cracking Unit (FCCU Source ID 101)
 - a) CO and SO₂ (measured via CEMS) and Liquid to Gas Ratio (in lieu of PM),
- 2) Sulfur Recovery Unit (SRU Source ID 102)
 - a) SO₂ (measured via CEMS)
- 3) Catalytic Reforming Unit (Platformer Unit Source ID 119)
 - a) Chloride levels on catalyst on the catalyst entering and exiting the Platformer Gas Adsorption system
 - b) Daily Average Vet Gas Inlet Temperature < 350 °F
- 4) Bypass lines serving the above units
 - a) Platformer and SRU have bypass lines, FCC does not.

As required under §63.1575(d) and (e), the following information is provided for the FCC and SRU:

- (d)(1) The total operating time of each affected source during the reporting period: $\underline{\text{See Attachment}}$ $\underline{1}$.
- (d)(2) Information on the number, duration, and cause of deviations (including unknown cause, if applicable), as applicable, and the corrective action taken: See Attachment 2. If no deviations are listed in the attachment, the monitored parameter was in compliance with the applicable requirement.
- (d)(3) Information on the number, duration, and cause for monitor downtime incidents (including unknown cause, if applicable, other than downtime associated with zero and span and other daily calibration checks): See Attachment 1.
- (e)(1) The date and time that each malfunction started and stopped: See Attachment 2.
- (e)(2) The date and time that each continuous opacity monitoring system or continuous emission monitoring system was inoperative, except for zero (low-level) and high-level checks: <u>See Attachment 1.</u>
- (e)(3) The date and time that each continuous opacity monitoring system or continuous emission monitoring system was out-of-control, including the information in §63.8(c) (8): See Attachment 1.
- (e)(4) The date and time that each deviation started and stopped, and whether each deviation occurred during a period of startup, shutdown, or malfunction or during another period: <u>See Attachment 2</u>.

- (e)(5) A summary of the total duration of the deviation during the reporting period (recorded in minutes for opacity and hours for gases and in the averaging period specified in the regulation for other types of emission limitations), and the total duration as a percent of the total source operating time during that reporting period: See Attachment 1
- (e)(6) A breakdown of the total duration of the deviations during the reporting period and into those that are due to startup, shutdown, control equipment problems, process problems, other known causes, and other unknown causes: See Attachment $\underline{1}$
- (e)(7) A summary of the total duration of downtime for the continuous opacity monitoring system or continuous emission monitoring system during the reporting period (recorded in minutes for opacity and hours for gases and in the averaging time specified in the regulation for other types of standards), and the total duration of downtime for the continuous opacity monitoring system or continuous emission monitoring system as a percent of the total source operating time during that reporting period: See Attachment 1.
- (e)(8) A breakdown of the total duration of downtime for the continuous opacity monitoring system or continuous emission monitoring system during the reporting period into periods that are due to monitoring equipment malfunctions, non-monitoring equipment malfunctions, quality assurance/quality control calibrations, other known causes, and other unknown causes: <u>See</u> Attachment 1
- (e)(9) An identification of each HAP that was monitored at the affected source: See Attachment 1.
- (e)(10) A brief description of the process units: See Attachment 3
- (e)(11) The monitoring equipment manufacturer(s) and model number(s): See Attachment 1.
- (e)(12) The date of the latest certification or audit for the continuous gas analysis system or continuous emission monitoring system: See Attachment $\underline{1}$.
- (e)(13) A description of any change in the continuous emission monitoring system or continuous opacity monitoring system, processes, or controls since the last reporting period: <u>See Attachment 1</u>.

Start-up, Shutdown, and Malfunction Plans (SSMP)

Any startup, shutdown, and malfunction at the Facility which occurred during the reporting period were managed consistent with the facility's SSMP.

40 CFR Part 60 Subpart J

The NSPS J Regulations emission standards regulate the following refinery affected sources and parameters:

- 1) Fluidized Catalytic Cracking Unit (FCCU Source ID 101)
 - a) CO and SO₂ (measured via CEMS) and Liquid to Gas Ratio (in lieu of PM),
- 2) Sulfur Recovery Unit (SRU Source ID 102) SO₂ (measured via CEMS)
- 3) Main Flare (Source ID 103) H₂S (measured via CEMS)
- 4) Sour Gas Flare (Source ID 121) H₂S (measured via CEMS)
- 5) North Side Fuel System Consumers (listed below) H₂S (measured via CEMS) Boiler 9 (Source ID 034); Kero Heater (Source ID 735); 543 Crude Heater (Source ID 744); Boiler 10 (Source ID 035); Diesel HTU Heater (Source ID 736); 544 Crude Heater (Source ID 745); Boiler 14 (Source ID 053); 541 Vac Heater (Source ID 742); 544 Vac Heater (Source ID 746); FCC Feed Heater (Source ID 733); and 542 Vac Heater (Source ID 743)
- 6) South Side Fuel System Consumers (listed below) H₂S (measured via CEMS) Naphtha Heater (Source ID 737); Platformer Feed Heater (Source ID 738); Isocracker 1st Stage Heater (Source ID 739); Isocracker Splitter Reboiler (Source ID 740) D2 VGO Hydrotreater Feed Heater (Source ID 741).

In accordance with 40 CFR 60.7(d), the excess emissions and monitoring system summary report is included in Attachment 1. If excess emissions are greater than 1%, or total CMS downtime is greater than 5%, the excess emission report per 40 CFR 60.7(c) is included in Attachment 4.

		Summary Report
Attachment 1: Excess Emissions and	Monitoring System Performance	Jummary Mepers
Attachment 1: Excess Emissions and		Jummary Nepers
Attachment 1: Excess Emissions and		Jummary Hepers
Attachment 1: Excess Emissions and		Jummary Hepers
Attachment 1: Excess Emissions and		Juninary Repers
Attachment 1: Excess Emissions and		Julimiary Hepers
Attachment 1: Excess Emissions and		Juninary Report
Attachment 1: Excess Emissions and		Juninary Repers
Attachment 1: Excess Emissions and		Juninary reper-
Attachment 1: Excess Emissions and		

Pollutant (Circle One):	SO ₂	NO_X	TRS	H ₂ S	CO	Opacity
Reporting period dates:	From	July 1, 2014			to	December 31, 2014
Company: Monroe En	ergy, LLC					
Emission Limitation:	500 ppm (1	hour average)				
Address: 4101 Post I	Rd, Trainer P	A 19061				
Monitor Manufacturer:	Servomex					
Model No.:	04900C1-42	202				
Date of Latest CMS Certific	ation or Audi	t: 12/16/20	14 (Linea	rity Test)	
Process Unit(s) Description	: FCCU					
Total source operating time	e in reporting	period ¹ : 4,2	88 hours			
Emission data summary 1			CMS	perform	ance s	ummary ¹
 Duration of excess emiss due to: 	sions in the re	porting period	34			the reporting period due to:

Emission data summary 1		CMS performance summary 1	
 Duration of excess emissions in the repo due to: Startup/shutdown 	rting period 0	CMS downtime in the reporting period du a. Monitor equipment malfunctions	e to:
 b. Control equipment problems 	0	b. Non-Monitor equipment malfunctions	
c. Process problems	0	c. Quality assurance calibration	
d. Other known causes			70
e. Unknown causes	0	d. Other known causes e. Unknown causes	0
2. Total duration of excess emissions	0		0
		2. Total CMS Downtime	79
 Total duration of excess emissions x (100) / [Total source operating time] 	0.0 % ²	3. [Total CMS Downtime] x (100) / [Total source operating time]	1.8 %

For opacity, record all times in minutes. For gases, record all times in hours.

For the reporting period: If the total duration of excess emissions is 1 percent or greater of the total operating time or the total CMS downtime is 5 percent or greater of the total operating time, both the summary report form and the excess emission report described in 40 CFR 60.7(c) shall be submitted.

Pollutant (Circle One):	SO ₂	NO_X	TRS	H ₂ S	СО	Opacity
Reporting period dates:	From	July 1, 202	14		_ to	December 31, 2014
Company: Monroe Er	ergy, LLC				3100 mark 24 5 m	
Emission Limitation:	50 ppm (7-	day rolling A	verage); 2	25 ppm (36	55-day r	olling average)
Address: 4101 Post	Rd, Trainer P	A 19061			<u> </u>	
Monitor Manufacturer:	AMETEK N	1odel 921				
Model No.:	Model 921					
Date of Latest CMS Certi	fication or Au	dit: 6/28	3/2014 (Lin	earity Tes	t)	
Process Unit(s) Descripti	on: FCCU					
Total source operating ti	me in reporti	ng period ¹ :	4,288 h	ours		-

Emission data summary ¹		CMS performance summary 1				
1. Duration of excess emissions in the report	ing period	1. CMS downtime in the reporting period due	to:			
due to:	0	a. Monitor equipment malfunctions	62			
a. Startup/shutdown	0	b. Non-Monitor equipment malfunctions	0			
 Control equipment problems 		c. Quality assurance calibration	11			
c. Process problems	0	and the state of t	0			
d. Other known causes	0	d. Other known causes	0			
e. Unknown causes	0	e. Unknown causes				
Total duration of excess emissions	0	2. Total CMS Downtime	73			
 Total duration of excess emissions x (100) / [Total source operating time] 	0.0 %	3. [Total CMS Downtime] x (100) / [Total source operating time]	1.7 %			

For opacity, record all times in minutes. For gases, record all times in hours.

For the reporting period: If the total duration of excess emissions is 1 percent or greater of the total operating time or the total CMS downtime is 5 percent or greater of the total operating time, both the summary report form and the excess emission report described in 40 CFR 60.7(c) shall be submitted.

			Table 1900 Comment of the			
Pollutant (Circle One):	(SO ₂)	NO _X	TRS	H ₂ S	СО	Opacity
Reporting period dates:	From	July 1, 2014			to	December 31, 2014
Company: Monroe Er	nergy, LLC					
Emission Limitation:	250 ppm (12	hour Rolling	Average			
Address: 4101 Post	Rd, Trainer PA	19061				
Monitor Manufacturer:	AMETEK					
Model No.:	Model 921					
Date of Latest CMS Certifi	cation or Audit	:: _12/17/2	2014 (Line	earity Test)	
Process Unit(s) Description	n: _Claus Su	ılfur Recovery	/ Plant		0.000	
Total source operating tim	e in reporting	period ¹ : 4,	416 houi	rs -		

Emission data summary 1		CMS performance summary 1	
 Duration of excess emissions in the repo due to: 	orting period	CMS downtime in the reporting period du	e to:
a. Startup/shutdown	0	a. Monitor equipment malfunctions	
 b. Control equipment problems 	0	b. Non-Monitor equipment malfunctions	47
c. Process problems	0		0
d. Other known causes	0	c. Quality assurance calibration	7
e. Unknown causes	0	d. Other known causes	0
2. Total duration of excess emissions		e. Unknown causes	0
	0	2. Total CMS Downtime	54
 Total duration of excess emissions x (100) / [Total source operating time] 	0.0 % ²	3. [Total CMS Downtime] x (100) / [Total source operating time]	1.2 %

For opacity, record all times in minutes. For gases, record all times in hours.

For the reporting period: If the total duration of excess emissions is 1 percent or greater of the total operating time or the total CMS downtime is 5 percent or greater of the total operating time, both the summary report form and the excess emission report described in 40 CFR 60.7(c) shall be submitted.

Pollutant (Circle One):	SO ₂	NO_X	TRS	H ₂ S	CO	Opacity
Reporting period dates:	From	July 1, 20	14		to_	December 31, 2014
Company: Monroe Er	nergy, LLC					
Emission Limitation:	162 ppm H	₂ S (3 Hour A	verage)			
Address: 4101 Post	Rd, Trainer F	A 19061				
Monitor Manufacturer:	Applied A	utomation				
Model No.:	AV4070					
Date of Latest CMS Certi	fication or Au	dit: _ 12/ 0	05/2014 (l	inearity Tes	st)	
Process Unit(s) Descripti	on: Nort	n Fuel Gas S	ystem			
Total source operating t	ime in report	ng period 1:	4,416 h	ours		

Emission data summary ¹		CMS performance summary 1		
Duration of excess emissions in the report	ing period	1. CMS downtime in the reporting period due to:		
due to:	0	a. Monitor equipment malfunctions	7	
a. Startup/shutdown		b. Non-Monitor equipment malfunctions	0	
b. Control equipment problems	0	c. Quality assurance calibration	2	
c. Process problems	4		0	
d. Other known causes	0	d. Other known causes	0	
e. Unknown causes	0	e. Unknown causes	9	
Total duration of excess emissions	0	Total CMS Downtime	9	
3. Total duration of excess emissions x (100) / [Total source operating time]	0.1 % ²	3. [Total CMS Downtime] x (100) / [Total source operating time]	0.2	%

For opacity, record all times in minutes. For gases, record all times in hours.

For the reporting period: If the total duration of excess emissions is 1 percent or greater of the total operating time or the total CMS downtime is 5 percent or greater of the total operating time, both the summary report form and the excess emission report described in 40 CFR 60.7(c) shall be submitted.

Pollutant (Circle One):	SO ₂	NO _x	TRS	H ₂ S	СО	Opacity
Reporting period dates:	From	July 1, 201	14		to .	December 31, 2014
Company: Monroe Er	nergy, LLC					
Emission Limitation:	162 ppm H ₂	S (3 Hour Av	erage)		1.762	
Address: 4101 Post	Rd, Trainer P	A 19061				
Monitor Manufacturer:	Applied Au	tomation				
Model No.:	AV4071					
Date of Latest CMS Certifi	cation or Aud	it: 12/10	/2014 (Lin	earity Test)		
Process Unit(s) Descriptio	n: South I	uel Gas Syst	tem			
Total source operating tim	ne in reporting	period 1:	4,416 hou	ırs		

Emission data summary 1		CMS performance summary 1	
 Duration of excess emissions in the repo due to: 	rting period	CMS downtime in the reporting period du	e to:
f. Startup/shutdown	0	a. Monitor equipment malfunctions	26
g. Control equipment problems	0	b. Non-Monitor equipment malfunctions	0
h. Process problems	0	c. Quality assurance calibration	
i. Other known causes	0	d. Other known causes	2
. Unknown causes	0	e. Unknown causes	0
Total duration of excess emissions	0	2. Total CMS Downtime	28
 Total duration of excess emissions x (100) / [Total source operating time] 	0.0 %2	3. [Total CMS Downtime] x (100) / [Total source operating time]	0.6 %

For opacity, record all times in minutes. For gases, record all times in hours.

For the reporting period: If the total duration of excess emissions is 1 percent or greater of the total operating time or the total CMS downtime is 5 percent or greater of the total operating time, both the summary report form and the excess emission report described in 40 CFR 60.7(c) shall be submitted.

Pollutant (Circle One): SO ₂ N	O _X TRS	H ₂ S	CO Opacity	
	1, 2014	to	December 31, 2014	
Company: Monroe Energy, LLC				
Emission Limitation: 162 ppm H2S (3 h	nour Average)			
Address: 4101 Post Rd, Trainer PA 190	61			
Monitor Manufacturer: Emerson P	rocess Manage	ment		
Model No.: Daniel 500 GC				
Date of Latest CMS Certification or Audit:	12/11/2	014 (Linearity T	est)	
Process Unit(s) Description: Ma	in Flare	7-2		
Total source operating time in reporting per	riod ¹ :	4,416 hours		
Emission data summary ¹		CMS performa	ance summary ¹	
Duration of excess emissions in the repo	rting period	1 CMS downt	ime in the reporting period du	e to:
due to:				11
a. Startup/shutdown	0		uipment malfunctions or equipment malfunctions	0
b. Control equipment problems	0			15
c. Process problems	0		urance calibration	0
d. Other known causes	3,634	d. Other know		0
e. Unknown causes	0	e. Unknown c		26
2. Total duration of excess emissions	0	2. Total CMS I		
3. Total duration of excess emissions x (100) / [Total source operating time]	82.3 % ²	3. [Total CMS source operat	Downtime] x (100) / [Total ting time]	0.6 % ²

For opacity, record all times in minutes. For gases, record all times in hours.

For the reporting period: If the total duration of excess emissions is 1 percent or greater of the total operating time or the total CMS downtime is 5 percent or greater of the total operating time, both the summary report form and the excess emission report described in 40 CFR 60.7(c) shall be submitted. See Attachment 4.

Pollutant (Circle One): SO ₂	NO _X T	RS H₂S CO Opacity
Reporting period dates: From	July 1, 2014	to <u>December 31, 2014</u>
Company: Monroe Energy, LLC		
Emission Limitation: 162 ppm H ₂ S	(3 hour Average	e)
Address: 4101 Post Rd, Trainer PA	19061	
Monitor Manufacturer: Emerso	n Process Mana	agement
Model No.: Daniel 500 G	С	
Date of Latest CMS Certification or Audit	5/21/	2014 (Linearity Test)
Process Unit(s) Description:S	our Gas Flare	
Total source operating time in reporting p	period ¹ :	4,416 hours
Emission data summary 1		CMS performance summary ¹
1. Duration of excess emissions in the rep	orting period	
due to: f. Startup/shutdown		CMS downtime in the reporting period due to:
f. Startup/shutdown g. Control equipment problems	0	a. Monitor equipment malfunctions 106
h. Process problems	0	b. Non-Monitor equipment malfunctions 0
i. Other known causes	0	c. Quality assurance calibration 0
j. Unknown causes	0	d. Other known causes 0
Total duration of excess emissions	0	e. Unknown causes 0
	0	2. Total CMS Downtime 106
 Total duration of excess emissions x (100) / [Total source operating time] 	0.0 % ²	3. [Total CMS Downtime] x (100) / [Total source operating time] 3.8 % ²

For opacity, record all times in minutes. For gases, record all times in hours.

For the reporting period: If the total duration of excess emissions is 1 percent or greater of the total operating time or the total CMS downtime is 5 percent or greater of the total operating time, both the summary report form and the excess emission report described in 40 CFR 60.7(c) shall be submitted.

Attachment 2 - Deviation Information

North Fuel Gas System (and associated consumers) 3-hour H_2S Concentration < 162 ppm

Source: Standard:

Contraction Action	Corrective Action Taken?		Amine circulation rates were increased and/or fresh amine was added to the system.				
Nature and Cause of Event?		High concentration (greater than 162	ppm, 3-hour rolling average) H2S in the	north side fuel gas system, unknown cause			
Caused by SSM event?		No					
Duration		1 hour		3 hours			
Stop		09/06/2014 16:00	1	09/07/2014			
Start	00/00/2011	15:00	. 100/100	14:00			

Attachment 3-Process Descriptions

FCCU Process Description

The Fluidized Catalytic Cracking Unit (FCCU) is a refinery process unit used for the production of gasoline. Heavy oil, which is used as the feedstock, is catalytically cracked in a fluidized catalyst bed to produce C3 olefins, C4 olefins, and isobutanes. In the cracking reactor, heavy carbonaceous materials (coke) become deposited on the catalyst, requiring continuous regeneration. The catalyst is circulated to a fluidized bed regenerator where these deposits are combusted. Most of the catalyst particles entrained in the regenerator flue gas are then removed in two stages of cyclones within the regenerator vessel and then are returned to the fluidized bed reactor.

At the Trainer Refinery, the FCCU control devices include a CO Boiler for CO reduction, an Enhanced Selective Non-Catalytic Reduction (eSNCR) unit for NO_x reduction, an electrostatic precipitator for PM reduction and a wet gas scrubber for PM and SO_2

Catalytic Reforming Unit (Platformer Unit)

The refinery operates one Catalytic Reforming Unit. The purpose of the Platformer is to upgrade low octane feed sources, Heavy Naphtha and Heavy Isocrackate, into a high-octane gasoline component and hydrogen gas. The feed combined with hydrogen recycle gas is heated and passed over a platinum catalyst, where it is converted from low octane naphtha to a gasoline-blending component with a design research octane number in the range of 97 - 101.

SRU

The Claus Sulfur Recovery Unit is designed to react feed H_2S and SO_2 into recoverable sulfur using two trains in parallel. Normally only one train is required to be on-line. The feeds to the unit are sour water gases and acid gases from the Sour Water Stripper and the Amine Unit. Each train consists of a thermal reactor, three catalytic reactors, a steam generator and a 4 pass sulfur condenser. Medium and low-pressure steam is generated in the condensers. The sulfur product is stored in a common heated pit until shipped out by railcar.

The Scot unit is designed to treat the tail gas from both trains of the Sulfur Recovery Unit. The Scot Unit reduces the H_2S content in the tail gas before it is sent to the incinerator stack. The combination of the Sulfur and Scot Units recovers about 99.8% of the sulfur in the feed streams. The Scot Unit consists of an in-line burners, catalytic reactor, quench tower, amine absorber, stripper, and incinerator.

Bypass Lines

The FCCU does not have any bypass lines. The Platformer Chlorsorb Unit line was not bypassed during this reporting period. The Sulfur Recovery Unit line was not bypassed during this reporting period.

Attachment 4 – Excess Emissions and Monitoring Systems Performance Report (40 CFR 60.7 (c))



Start Date/Time	End Date/Time	Magnitude of Emissions (ppm H₂S)	SSM Related?	Nature and Cause of Malfunction	Corrective Action Taken/Preventative Measures
07/01/14 00:00	07/01/14 09:00	170.2-188.2			
07/01/14 16:00	07/02/14 00:00	170.0-458.6			
07/02/14 04:00	07/02/14 16:00	170.9-206.5			
07/10/14 13:00	07/10/14 17:00	169.6-274.5			
07/15/14 11:00	07/15/14 22:00	186.8-555.4			
07/16/14 12:00	08/15/14 21:00	165.9-1790.2			
08/15/14 23:00	08/28/14 15:00	171.0-2126.4			
08/29/14 02:00	09/19/14 09:00	176.9-1471.4		1	
09/19/14 13:00	10/10/14 18:00	191.8-2055.0			
10/10/14 21:00	10/12/14 14:00	174.8-347.1			
10/13/14 22:00	10/14/14 04:00	162.7-279.0			
10/14/14 06:00	10/14/14 09:00	177.5-181.5	1	8	
10/14/14 19:00	10/15/14 03:00	163.4-176.6			1
10/15/14 10:00	10/15/14 15:00	165.6-219.2			
10/18/14 14:00	10/19/14 20:00	165.4-302.2			
10/20/14 16:00	11/02/14 00:00	162.5-411.1			Flare Gas Recovery
11/02/14 01:00	11/02/14 05:00	163.9-667.3			
11/02/14 01:00	11/03/14 18:00	171.1-311.5			
11/03/14 17:00	11/04/14 15:00	177.1-229.4	No	N/A	Unit Was installed
11/05/14 21:00	11/05/14 16:00	164.5-225.3			
11/05/14 18:00	11/08/14 07:00	162.0-407.1			
11/03/14 18:00	11/09/14 21:00	168.6-664.5			
11/11/14 08:00	11/11/14 11:00	162.2-165.1			
11/11/14 08:00	11/13/14 12:00	165.3-176.5			
11/13/14 08:00	11/14/14 18:00	163.7-196.2			
11/15/14 07:00	11/15/14 12:00	163.9-171.4			
11/16/14 09:00	11/16/14 10:00	180.4-182.1		4	
11/16/14 23:00	11/17/14 01:00	163.4-164.6			
11/17/14 19:00	11/18/14 00:00	162.1-173.6			
11/18/14 08:00	11/18/14 19:00	163.2-184.0			
11/19/14 01:00	11/19/14 03:00	163.4-167.4			
11/19/14 07:00	11/19/14 10:00	179.1-194.4			
11/19/14 07:00	11/19/14 18:00	189.2			
11/20/14 17:00	11/20/14 18:00	162.1-619.1			
11/20/14 12:00	12/11/14 15:00	173.9-1025.2	2		
12/11/14 19:00	12/13/14 11:00	414.0-601.9			
12/13/14 19:00	01/01/15 00:00	171.0-539.7			